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(54) Title: AROMATIC ALKYLATION WITH ALPHA-OLEFIN DIMER

(57) Abstract

A process is disclosed for the production of novel monoalkylbenzenes or substituted benzenes by aromatics alkylation wherein the alkylation catalyst is an acidic shape selective metallosilicate catalyst and the alkylating agent is the olefinic dimer by-product of the oligomerization of alpha-olefins in contact with reduced valence state solid chromium oxide catalyst on a porous support. The alkylated benzenes produced comprise those mono-alkylbenzenes wherein the alkyl group contains 12 to 28 carbon atoms and have high viscosity index, low pour point and low viscosity. They have a low degree of residual olefinic unsaturation and are useful as additives to thermally and oxidatively stabilize lubricant materials. The process comprises reacting benzene or substituted benzene with C₆-C₁₄ alpha-olefin olefinic dimer having a branch ratio of less than 0.19, or mixture of the dimers, in contact with acidic shape selective zeolite catalyst having large pore size.

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AROMATIC ALKYLATION WITH ALPHA-OLEFIN DIMER

This invention relates to a process for the preparation of synthetic oils useful as lubricants, lubricant additives and insulating fluids. More particularly, the invention relates to a 5 process for the monoalkylation of aromatic hydrocarbons with novel olefins obtained from the oligomerization of C₆-C₂₀ alpha-olefins where the alkylating agent is the alpha-olefin oligomerization dimer.

It has been well established in the prior art that 10 hydrocarbon oils possessing superior properties in applications such as low viscosity lubricants, insulating fluids for electrical transformers, additives for lubricants, and the like can be prepared by alkylation of aromatic compounds using higher molecular weight olefins and olefinic oligomers.

15 U.S. patent 4,238,343 to Pellegrini, Jr. discloses a synthetic oil composition useful as an insulating fluid in electrical apparatus comprising the mono or di-alkylation product from the alkylation of aromatics with oligomers containing at least 30 and up to 60 carbon atoms. The oligomers are prepared by 20 Lewis acid catalysis by methods well known in the art. The alkylation reaction is conducted using conventional liquid Lewis acid catalyst and the degree of substitution is controlled by the aromatic to olefin mole ratio. Dimers are separated from oligomers and not included in the alkylation reaction.

25 U. S. patent 4,604,491 to Dressler et al. discloses a synthetic oil composition for functional fluids such as lubricants, heat transfer fluids, vacuum pump oils, etc. The compositions comprise mono and polyalkylated naphthalenes prepared by the alkylation of naphthalene with alpha-olefins in 30 contact with high silica zeolites. The alkyl substituent on naphthalene contains between 12 and 26 carbon atoms.

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U.S. patent 4,714,794 to Yoshida et al. discloses a synthetic oil composition comprising monoalkylated naphthalene obtained by alkylation of naphthalene with alkyl halide, alcohol or a straight chain mono-olefin having six to twenty four carbon atoms. The mole ratio of alpha to beta substitution on naphthalene is at least 1.0. The products exhibit high oxidation stability.

Recently, novel lubricant compositions (referred to herein as HVI-PAO) comprising polyalpha-olefins and methods for their preparation employing as catalyst reduced chromium on a silica support have been disclosed in U.S. patents 4,827,064 and 4,827,073. The process comprises contacting C_6-C_{20} 1-alkene feedstock with reduced valence state chromium oxide catalyst on porous silica support under oligomerizing conditions in an oligomerization zone whereby high viscosity, high viscosity index (VI) liquid hydrocarbon lubricant is produced having branch ratios less than 0.19 and pour point below -15°C. The process is distinctive in that little isomerization of the olefinic bond occurs compared to known oligomerization methods to produce polyalpha-olefins using Lewis acid catalyst. Lubricants produced by the process cover the full range of lubricant viscosities and exhibit a remarkably high viscosity index (VI) and low pour point even at high viscosity. The as-synthesized HVI-PAO oligomer has a preponderance of terminal olefinic unsaturation.

In the preparation of the novel HVI-PAO lubricant, alpha-olefin dimer containing olefinic unsaturation can be separated from the oligomerization reaction. The composition of the dimer mixture conforms to the unique specificity of the oligomerization reaction in that little double bond isomerization is found and shows a low branch ratio.

It has been found that novel monoalkylbenzenes or substituted benzenes can be produced by an aromatics alkylation

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process wherein the alkylation catalyst used is an acidic shape selective metallosilicate catalyst and the alkylating agent is the olefinic dimer by-product of the oligomerization of alpha-olefins in contact with reduced valence state solid chromium oxide catalyst on a portus support. The olefinic dimer is the by-product of an oligomerization process notable for the very low degree of double bond isomerization occurring during the reaction such that the oligomer hydrocarbons and dimer by-products produced show branch ratios below 0.19. The alkylated benzenes produced comprise those mono-alkylbenzenes wherein the alkyl group contains 12 to 28 carbon atoms.

It has been further found that the monoalkylbenzenes of the present invention have high viscosity indices, low pour point and low viscosity. They have a low degree of residual olefinic unsaturation and are useful as additives to thermally and oxidatively stabilize lubricant materials. They are, of themselves, useful as low viscosity lubricants.

More particularly, a process is disclosed for the production of aromatic hydrocarbon synthetic oil comprising the steps of:

contacting C₆-C₁₄ alpha olefin with a supported solid reduced metal oxide catalyst under oligomerization conditions at a temperature of 90 to 250°C, the metal oxide comprising a lower valence form of at least one Group VIB metal to produce lubricant range hydrocarbon product oligomers having a branch ratio of from 0.10 to 0.19 and a viscosity index of at least 130;

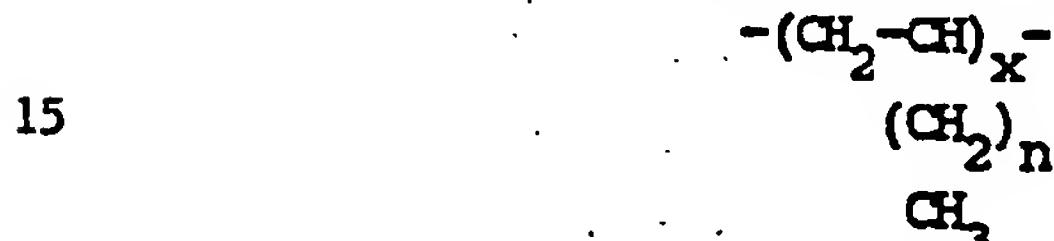
separating the oligomers and recovering C₁₂-C₂₈ olefinic dimer by-product by distillation; and

reacting benzene or substituted benzene with the dimer, or mixture of the dimer, in contact with acidic shape selective metallosilicate catalyst under alkylation conditions whereby mono-alkylbenzenes containing C₁₂-C₂₈ alkyl group are produced.

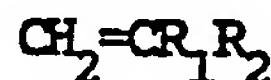
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In the present invention aromatic hydrocarbons are alkylated with unique olefin dimers produced as by-product in the oligomerization of 1-alkenes in contact with reduced chromium oxide on silica support. A characteristic of the novel
5 oligomerization reaction from which the by-product dimers used as alkylating agent in the present invention are produced is the production of mixtures of dialkyl vinylidenic and 1,2 dialkyl or trialkyl mono-olefin oligomers (referred to herein as HVI-PAO oligomers), as determined by
10 infra-red and nuclear magnetic resonance (NMR) analysis.

In general, the HVI-PAO oligomers have the following regular head-to-tail structure where n is preferably 0 to 17, terminating in olefinic unsaturation:



15 with some head-to-head connections. The HVI-PAO process produces a surprisingly simpler and useful dimer compared to the dimer produced by 1-alkene oligomerization with BF_3 or AlCl_3 , as
20 commercially practiced. Typically, in the present invention it has been found that a significant proportion of unhydrogenated dimerized 1-alkene, or alpha-olefin, has a vinylidanyl structure as follows:



25 where R_1 and R_2 are alkyl groups representing the residue from the head-to-tail addition of 1-alkene molecules. For example, the by-product dimer from 1-decene oligomerization according to the HVI-PAO process, which can be used as alkylating olefin in the present invention, has been found to contain three major
30 components, as determined by GC. Based on ^{13}C NMR analysis, the unhydrogenated components were found to be 8-eicosene, 9-eicosene, 2-octyldodecene and 9-methyl-8 or 9-methyl-9-nonadecene.

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Olefins suitable for use as starting material in the preparation of olefinic HVI-PAO oligomers and the by-product dimer used as starting material in the present invention include those olefins containing from 6 to 14 carbon atoms such as 5 1-hexene, 1-octene, 1-decene, 1-dodecene and 1-tetradecene and branched chain isomers such as 4-methyl-1-pentene. Also suitable for use are olefin-containing refinery feedstocks or effluents. However, the olefins used
10 in this invention are preferably alpha olefinic as for example 1-octene to 1-dodecene and more preferably 1-decene, or mixtures of such olefins.

HVI-PAO oligomers of alpha-olefins used in this invention have a low branch ratio of less than 0.19 and superior lubricating properties compared to the alpha-olefin oligomers 15 with a high branch ratio, as produced in all known commercial methods.

This class of unsaturated HVI-PAO alpha-olefin oligomers are prepared by oligomerization reactions in which a major proportion of the double bonds of the alpha-olefins are not 20 isomerized. These reactions include alpha-olefin oligomerization by supported metal oxide catalysts, such as Cr compounds on silica or other supported IUPAC Periodic Table Group VIB compounds. The catalyst most preferred is a lower valence Group VIB metal oxide on an inert support. Preferred supports include 25 silica, alumina, titania, silica alumina, magnesia and the like. The support material binds the metal oxide catalyst. Those porous substrates having a pore opening of at least 40×10^{-7} mm (40 angstroms) are preferred.

The support material usually has high surface area and 30 large pore volumes with average pore size of 40 to 350×10^{-7} mm (40 to 350 angstroms). The high surface area are beneficial for supporting large amount of highly dispersive, active chromium metal centers and to give maximum efficiency of metal usage,

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resulting in very high activity catalyst. The support should have large average pore openings of at least 40×10^{-7} mm (40 angstroms), with an average pore opening of >60 to 300×10^{-7} mm (>60 to 300 angstroms) preferred. This large pore opening will not impose any diffusional restriction of the reactant and product to and away from the active catalytic metal centers, thus further optimizing the catalyst productivity. Also, for this catalyst to be used in fixed bed or slurry reactor and to be recycled and regenerated many times, a silica support with good physical strength is preferred to prevent catalyst particle attrition or disintegration during handling or reaction.

The supported metal oxide catalysts are preferably prepared by impregnating metal salts in water or organic solvents onto the support. Any suitable organic solvent known to the art may be used, for example, ethanol, methanol, or acetic acid. The solid catalyst precursor is then dried and calcined at 200 to 900°C by air or other oxygen-containing gas. Thereafter the catalyst is reduced by any of several various and well known reducing agents such as, for example, CO, H₂, NH₃, H₂S, CS₂, CH₃SCH₃, CH₃SSCH₃, metal alkyl containing compounds such as R₃Al, R₃B, R₂Mg, RLi, R₂Zn, where R is alkyl, alkoxy, aryl and the like. Preferred are CO or H₂ or metal alkyl containing compounds. Alternatively, the Group VIB metal may be applied to the substrate in reduced form, such as CrII compounds. The resultant catalyst is very active for oligomerizing olefins at a temperature range from below room temperature to 250°C at a pressure of 10 kPa (0.1 atmosphere) to 34580 kPa (5000 psi). Contact time of both the olefin and the catalyst can vary from one second to 24 hours. The catalyst can be used in a batch type reactor or in a fixed bed, continuous-flow reactor.

In general the support material may be added to a solution of the metal compounds, e.g., acetates or nitrates, etc., and the mixture is then mixed and dried at room

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temperature. The dry solid gel is purged at successively higher temperatures to 600°C for a period of 16 to 20 hours. Thereafter the catalyst is cooled under an inert atmosphere to a temperature of 250 to 450°C and a stream of pure reducing agent is contacted therewith for a sufficiently long period to reduce the catalyst as indicated by a distinct color change from bright orange to pale blue. Typically, the catalyst is treated with an amount of CO equivalent to a two-fold stoichiometric excess to reduce the catalyst to a lower valence CrII state. Finally the catalyst is cooled to room temperature and is ready for use.

The product oligomers have a very wide range of viscosities with high viscosity indices suitable for high performance lubrication use. The product oligomers also have atactic molecular structure of mostly uniform head-to-tail connections with some head-to-head type connections in the structure. These low branch ratio oligomers have high viscosity indices at least 15 to 20 units and typically 30-40 units higher than equivalent viscosity prior art oligomers, which regularly have higher branch ratios and correspondingly lower viscosity indices. These low branch oligomers maintain better or comparable pour points.

The branch ratios, defined as the ratios of CH₃ groups to CH₂ groups in the reaction products and by-products, are calculated from the weight fractions of methyl groups obtained by infrared methods, published in Analytical Chemistry, Vol. 25, No. 10, p. 1466 (1953).

$$\begin{aligned} \text{Branch ratio} &= \frac{\text{wt fraction of methyl group}}{1 - (\text{wt fraction of methyl group})} \end{aligned}$$

The unique olefinic dimers used as alkylating agent in the present invention are produced as by-product of the HVI-PAO oligomerization reaction. Typically, in the production of HVI-PAO

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oligomer lubricant base stock, the oligomerization reaction mixture is separated from the catalyst and separated by vacuum distillation to remove unreacted alpha-olefin and lower boiling by-products of the oligomerization reaction, such as alpha-olefin dimer. This provides a lubricant basestock of suitably high volatility and viscosity. While other methods known to those skilled in the art, such as solvent extraction, may be used to separate the alpha-olefin dimer by-product, distillation is preferred.

In the process of the present invention to produce alkylated aromatics, particularly mono-alkylbenzenes, by alkylation with aforenoted dimer, suitable aromatic hydrocarbon starting materials include benzene, mono and di-alkylbenzenes, halobenzenes, alkoxybenzenes, carboxy and carbalkoxy benzenes, phenol, catechol, acetanilide, acetophenone, and the like. Preferred aromatics include benzene, toluene, chlorobenzene and anisole.

The alkylation reaction of the present invention is conducted by contacting a mixture of olefinic dimer and aromatic hydrocarbon with a solid shape selective acidic metallosilicate catalyst having a large pore size. The reaction may be conducted at a temperature between 0 and 300°C, but preferably between 160 and 200°C. The reaction pressure can be between 107 and 7000 kPa (1 psig and 1000 psig), but is preferably 2760 kPa (400 psig). The liquid hourly space velocity (LHSV) based on catalyst can be between .01 and 10, but is preferably between 0.4 and 0.6.

The alkylation reaction can be conducted with or without a solvent. Useful solvents include nitrobenzene, tetrahydrofuran, perchlorobenzene and all such generally higher boiling solvents inert in the alkylation reaction. However, it is preferable to conduct the reaction in the absence of added solvent and more

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preferable to employ an excess of aromatic hydrocarbon reactant as solvent. The process of the present invention can be carried out to produce mono-alkylbenzenes using a mole ratio of reactant benzenes to olefinic dimer alkylating agent of between 50:1 and 5 0.5:1, preferably between 5:1 and 1:1. The reaction can be carried out in any vessel suitable for the reaction between fluid alkylating agent and benzenes with solid catalyst. Preferably, the reaction is conducted in a fixed bed reactor or a continuous stirred tank reactor but may be effectively carried out in a 10 batch reactor.

Surprisingly, the process of the present invention leads to essentially mono alkylation of aromatic hydrocarbon with olefinic dimer when the alkylation is carried out using acidic shape selective metallocosilicate catalyst such as aluminosilicate 15 zeolite. The shape selective characteristics of zeolite catalysts are well known to those skilled in the art and in the present invention such shape selectivity is deemed to have a determining influence in the surprising limitation of the reaction products to essential monoalkylates. The application of shape-selective 20 catalysis is discussed in "Industrial Application of Shape Selective Catalysis" by N. Y. Chen and W. E. Garwood in Catal. Rev. Sci. Eng., 28(2&3), 185-264 (1986).

Zeolites of interest to shape selective catalysis are divided into three major groups according to their pore/channel 25 systems. These systems include 8-membered oxygen ring systems, 10-membered oxygen ring systems and dual pore systems including 12-membered oxygen ring openings. In general, they are referred to as small, medium or large pore size zeolites proceeding from 8 to 12 membered ring systems. The systems are more completely 30 described in Atlas of Zeolite Structures Types, International Zeolite Assoc., Polycrystal Book Service, Pittsburg, 1978.

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Zeolites useful as catalysts in the present invention include all natural or synthetic acidic large pore size zeolites, typically with a pore size of $6.4 \text{ to } 7.5 \times 10^{-7} \text{ mm}$ (6.4 to 7.5 Angstroms). Particularly useful catalysts include the acidic form of ZSM-4, ZSM-12, ZSM-20, Faujasite X & Y with pore size of $7.4 \times 10^{-7} \text{ mm}$ (7.4 Angstroms) Cancrinite, Gmelinite, Mazzite, Mordenite and Offretite. A preferred catalyst is Faujasite Y.

The following examples are presented to illustrate the present invention and are not intended to limit the scope of the invention.

Example 1

Catalyst Preparation and Activation Procedure

1.9 grams of chromium (II) acetate ($\text{Cr}_2(\text{OCOCH}_3)_4 \cdot 2\text{H}_2\text{O}$) (5.58 mmole) (commercially obtained) is dissolved in 50 ml of hot acetic acid. Then 50 grams of a silica gel of 8-12 mesh size, a surface area of $300 \text{ m}^2/\text{g}$, and a pore volume of 1 ml/g, also is added. Most of the solution is absorbed by the silica gel. The final mixture is mixed for half an hour on a rotavap at room temperature and dried in an open-dish at room temperature. First, the dry solid (20 g) is purged with N_2 at 250°C in a tube furnace. The furnace temperature is then raised to 400°C for 2 hours. The temperature is then set at 600°C with dry air purging for 16 hours. At this time the catalyst is cooled under N_2 to a temperature of 300°C . Then a stream of pure CO (99.99% from Matheson) is introduced for one hour. Finally, the catalyst is cooled to room temperature under N_2 and ready for use.

Example 2

30 The catalyst prepared in Example 1 (3.2 g) is packed in a 9.5mm (3/8") stainless steel tubular reactor inside an N_2 blanketed dry box. The reactor under N_2 atmosphere is then

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heated to 150°C by a single-zone Lindberg furnace. Pre-purified 1-hexene is pumped into the reactor at 1070 kPa (140 psi) and 20 ml/hr. The liquid effluent is collected and stripped of the unreacted starting material and the low boiling material at 5 kPa (0.05 mm Hg). The residual clear, colorless liquid has viscosities and VI's suitable as a lubricant base stock.

	<u>Sample</u>	<u>Prerun</u>	<u>1</u>	<u>2</u>	<u>3</u>
	T.O.S.*, hr.	2	3.5	5.5	21.5
	Lube Yield, wt%	10	41	74	31
10	Viscosity, mm ² /s (cS)				
	at 40°C	208.5	123.3	104.4	166.2
	100°C	26.1	17.1	14.5	20.4
	VI	159	151	142	143

*Time on stream

15

Example 3

A commercial chrome/silica catalyst which contains 1% Cr on a large-pore volume synthetic silica gel is used. The catalyst is first calcined with air at 800°C for 16 hours and reduced with CO at 300°C for 1.5 hours. Then 3.5 g of the catalyst is packed into a tubular reactor and heated to 100°C under the N₂ atmosphere. 1-Hexene is pumped through at 28 ml per hour at 101 kPa (1 atmosphere). The products are collected and analyzed as follows:

	<u>Sample</u>	<u>C</u>	<u>D</u>	<u>E</u>	<u>F</u>
25	T.O.S.*, hrs.	3.5	4.5	6.5	22.5
	Lube Yield, %	73	64	59	21
	Viscosity, mm ² /s (cS),				
	at 40°C	2548	2429	3315	9031
	100°C	102	151	197	437
30	VI	108	164	174	199

*Time on stream

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Example 4

Five grams of an ammonium Faujacite Y zeolite is placed in a fixed bed reactor. The catalyst is bound with 35% silica. The reactor is heated in air to 538°C and maintained at this temperature for 12 hours. The ammonium Y zeolite is transformed to the hydrogen or acidic Y form. A feed comprised of benzene and by-product C₂₀ olefinic dimer from the oligomerization of 1-decene in the mole ratio of 5:1 benzene to dimers is passed over the catalyst at 2900 kPa (400 psig). The initial reaction 5 temperature is 160°C at an IHSV of 0.4. At these reaction conditions 88.1% of the dimers are reacted, according to gas chromatographic analysis. After distillation at 220°C and 660 Pa (5mm Hg), the product has the properties presented in Table 1.

10

Example 5

Using the same feed and catalyst as in Example 5, reaction was carried out at 200°C and 0.6 IHSV. Dimer conversion is 92.8%, according to gas chromatographic analysis. The product properties are presented in Table 1.

15

Infrared analysis of the mono-alkylbenzenes confirmed 20 that the structures are alkylbenzenes. IR spectra of a model compound, 1-phenyldodecane, when compared to the products made by this method is found to be identical.

Gas chromatographic analysis of the products further shows the presence of C₂₆ mono-alkyl benzenes. No di-substituted 25 products are noted by GC analysis.

The following elemental analysis and molecular weight determinations are consistent with mono alkyl substitution:

	% Carbon	% Hydrogen	M.W.
Example 5	87.23	13.38	385
Example 6	87.09	12.87	379
Calculated (monoalkyl)	87.15	12.85	358

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Table 1

Example	<u>5</u>	<u>6</u>
Temperature, °C	160	200
Pressure, kPa (psig)	2860 (400)	2860 (400)
LHSV	0.4	0.6
% Conversion of Dimer	88.1	92.8
ALKYLATE PROPERTIES		
KV, 40°C	17.80	15.47
KV, 100°C	3.86	3.47
Viscosity Index	108.7	99.4
Bromine Number	2.4	4.4
Pour Point, °C	-35.7	-37.5

It has been found that the products of the present invention are useful as additives to mineral oil and synthetic oils when added to those oils in small but sufficient amounts. Lubricants are often formulated with additives to enhance properties for specific applications.

The more commonly used additives include oxidation inhibitors, rust inhibitors, metal passivators, antiwear agents, extreme pressure additives, pour point depressants, detergent-dispersants, viscosity index (VI) improvers, foam inhibitors and the like. This aspect of lubricant arts is specifically described in Kirk-Othmer "Encyclopedia of Chemical Technology", 3rd edition, Vol. 14, pp 477-526. Alkylated aromatics are known in the prior art as lubricant additives for their antiwear properties, thermal and oxidative stability as disclosed in U.S. Patents 4,211,665, 4,238,343, 4,604,491 and 4,714,794.

Although the present invention has been described with preferred embodiments and examples, it is to be understood that modifications and variations may be resorted to without departing from the spirit and scope of this invention, as those skilled in the art will readily understand. Such modifications and

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variations are considered to be within the purview and scope of
the following claims.

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CLAIMS:

1. A process for the production of mono-alkylbenzenes containing C₁₆-C₂₈ alkyl group from alpha-olefin dimer, comprising;

5 reacting benzene or substituted benzene with C₆-C₁₄ alpha-olefin olefinic dimer having a branch ratio of less than 0.19, or mixture of the dimers, in contact with acidic shape selective metallosilicate catalyst under alkylating conditions whereby the mono-alkylbenzenes are produced.

2. The process of claim 1 wherein the metallosilicate catalyst comprises acidic aluminosilicate zeolite-type catalyst containing large pore size.

3. The process of claim 2 wherein the catalyst comprises acidic zeolite containing pore size of 7.4 x 10⁻⁷ mm.

4. The process of claim 1 wherein the catalyst comprises acidic X or Y Faujasite.

5. The process of claim 1 wherein the alpha-olefin olefinic dimer comprises the reaction product of the process comprising:

5 contacting C₆-C₁₄ alpha olefin with a supported solid reduced metal oxide catalyst under oligomerization conditions at a temperature of 90 to 250°C, the metal oxide comprising a lower valence form of at least one Group VIB metal to produce lubricant range hydrocarbon product oligomers having a branch ratio of 0.10 to 0.19 and a viscosity index of at least 130;

\$ separating the oligomers and recovering the dimer fraction thereof by distillation.

10 6. The process of claim 5 wherein the supported solid reduced metal oxide catalyst comprises carbon monoxide reduced chromium oxide and the support comprises silica.

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7. The process of claim 5 wherein the alpha-olefins are taken from the group consisting essentially of 1-hexene, 1-octene, 1-decene, 1-dodecene and 1-tetradecene.

8. The process of claim 1 wherein the dimer comprises 1-decene dimer containing 20 carbon atoms.

9. The process of claim 1 wherein the monoalkyl benzenes comprise C₂₀ alkylbenzenes having a bromine number below 5, viscosity index greater than 90 and pour point below -30°C.

10. The process of claim 1 wherein the alkylating conditions comprise temperature between 0 and 300°C, pressure between 110 and 7000 kPa and liquid hourly space velocity between 0.01 and 10.

11. The process of claim 1 wherein the alkylating conditions comprise temperature between 160 and 200°C, pressure 2860 kPa and liquid hourly space velocity between 0.4 and 0.6.

INTERNATIONAL SEARCH REPORT

International Application No PCT/US 90/01714

I. CLASSIFICATION OF SUBJECT MATTER (if several classification symbols apply, indicate all)

According to International Patent Classification (IPC) or to both National Classification and IPC

IPC⁵: C 07 C 15/107, C 07 C 2/66, C 07 C 2/10

II. FIELDS SEARCHED

Minimum Documentation Searched ?

Classification System	Classification Symbols
IPC⁵	C 07 C 15/00, C 07 C 2/00

Documentation Searched other than Minimum Documentation
to the Extent that such Documents are Included in the Fields Searched *

III. DOCUMENTS CONSIDERED TO BE RELEVANT*

Category *	Citation of Document, ¹¹ with indication, where appropriate, of the relevant passages ¹²	Relevant to Claim No. ¹³
A	EP, A, 0017457 (MOBIL OIL CORPORATION) 15 October 1980 --	
A	US, A, 3631120 (P.E. EBERLY JR. et al.) 28 December 1971 --	
P,X	US, A, 4827073 (WU) 2 May 1989 see claims; example 22 (cited in the application)	5-7

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IV. CERTIFICATION

Date of the Actual Completion of the International Search

14th June 1990

Date of Mailing of this International Search Report

16 JUIL. 1990

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**ANNEX TO THE INTERNATIONAL SEARCH REPORT
ON INTERNATIONAL PATENT APPLICATION NO. US 9001714
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This annex lists the patent family members relating to the patent documents cited in the above-mentioned international search report.
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